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EP-A- 0 261 303
GB-A- 2 044 905
GB-A- 2 074 889

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Description

This invention relates to heating matter and is particularly, but not exclusively, applicable to methods of heating matter using apparatus as disclosed in specification EP-A-0068853 and copending British Specifications Nos. 2202618A, 2203670A, 2205049A and 2211597A, and in which matter is moved in a band continuously along an annular path in an annular zone by directing fluid flow into the zone over the annular extent thereof with both circumferential and vertical flow components. It will be understood that by utilising heated fluid for the fluid flow over at least a portion of the annular extent of the zone, there will be a heat transfer between the heated fluid and matter as the heated fluid passes through the band thereby heating the matter.

A gaseous mixture which is reactable to produce heat may be used to provide a heated fluid flow, for example the gaseous mixture may be a combustible gaseous mixture, typically comprising an air-gaseous fuel mixture. EP-A-0068853 discloses a method of heating matter comprising supplying said matter to a heating zone to be heated therein and providing in said heating zone a gaseous mixture which is reactable to produce heat and igniting said gaseous mixture within the extent of said matter to thereby provide a heated fluid flow in the heating zone.

However, it will be understood that, for the above process of producing a heated fluid flow to be efficient in a method of heating matter as described above, wherein the heated fluid flow passes through a band of the matter which is moving continuously along an annular path in an annular zone, the reaction which produces the heated fluid flow should occur in the zone and must be rapid to ensure that the reaction is substantially completed within the extent of the band, which for example is typically 50mm deep.

We have found that the required rapid reaction can be achieved by supplying the gaseous mixture at a temperature above that at which fuel dissociation occurs such that spontaneous ignition occurs and no flame front exists.

GB-A-2074889 discloses a method of heat treatment of foodstuffs in which a stream of oxygen-containing gas and fuel is passed over one or more catalysts to raise the temperature of the gas stream and the resulting hot gas stream is contacted with a foodstuff. In the method a preheated gaseous mixture (the fuel and oxygen-containing gas) is provided in a heating zone where it reacts in contact with a catalyst bed to produce a heated fluid flow. Matter to be heated (a cool airstream for cooling the heated fluid flow or the foodstuff) is supplied to the heating zone downstream of the

catalyst in which the heat producing reaction takes place.

The present invention provides a method of heating matter comprising supplying said matter to a heating zone to be heated therein and providing in said heating zone a gaseous mixture which is reactable to produce heat and igniting said gaseous mixture within the extent of said matter to thereby provide a heated fluid flow in the heating zone, characterised in that said gaseous mixture is provided in said heating zone at a temperature above that at which spontaneous ignition thereof occurs such that said gaseous mixture reacts, with no flame front being present during the reaction, within the extent of said matter.

Advantageously, the gaseous mixture comprises a combustible gaseous mixture and said heat producing reaction, with no flame front present, occurring in said heating zone is a combustion reaction.

Furthermore, in presently preferred embodiments the combustible gaseous mixture comprises an air-gaseous fuel mixture.

Although the invention is applicable to other methods of heating matter, it is especially applicable to the above-described method, in which case the matter to be heated is moved in a band continuously along an annular path in an annular zone by directing fluid flow into said zone over the annular extent thereof with both circumferential and vertical flow components, said fluid flow comprising said gaseous mixture over at least a portion of the annular extent of said zone, and the reaction thereof being substantially completed within the extent of said band.

The fluid flow may comprise said gaseous mixture over the annular extent of said zone.

The matter may comprise particulate material which forms a resident bed moving in said band along said annular path.

The gaseous mixture may be directed into a first annular region of said annular zone, which region is contiguous with and disposed inwardly of a second annular region of said annular zone such that said reaction occurs substantially in said first annular region, and said matter is circulated between said regions whilst moving in said band.

In embodiments of the invention described hereinafter the gaseous mixture comprises an air-gaseous fuel mixture and the fluid flow is directed into said annular zone through an annular inlet comprising an annular array of fixed inclined vanes arranged in overlapping relationship, said gaseous fuel being mixed with heated air immediately upstream of respective passages defined between said vanes and combustion occurring downstream of said vanes.

Preferably the air-gaseous fuel mixture is confined substantially to the region above the vanes by directing respective flows through said annular inlet at the radially inner and outer edges thereof with radially outwardly and radially inwardly flow components respectively.

The gaseous fuel may comprise natural gas, and in an embodiment of the invention an air-natural gas mixture is supplied at a temperature greater than 700 °C. The temperature of this mixture is obtained by mixing the natural gas with heated air at a temperature of less than about 1000 °C, for example between 850 and 900 °C.

In order that the invention may be better understood, some embodiments thereof will now be described, reference being had to the accompanying drawings, in which:

Figure 1 is a graph showing the effect of the temperature of an air-gaseous fuel mixture on combustion rate;

Figure 2 is a schematic axial cross-section of an apparatus for heating matter;

Figure 3 is a cross-section along the line III-III of Figure 2;

Figure 4 shows the portion indicated by IV in Figure 2 to a larger scale and in more detail than in Figure 2;

Figure 5 is a section taken along the line V-V in Figure 4 showing four blades of the apparatus;

Figure 6 is a top, part section view of three blades of the apparatus;

Figure 7 is a perspective view of a single blade of the apparatus;

Figure 8 is a schematic top plan view of another apparatus for heating matter taken along the line VIII-VIII of Figure 9; and

Figure 9 is an axial cross-section of the same apparatus.

Referring first to Figure 1, the effect of the temperature of a combustible air-gaseous fuel mixture prior to combustion on the rate of combustion is indicated. It will be noted that combustion of the mixture at the lowest temperature A is comparatively slower than combustion of the mixture at higher temperatures B and C, the temperature/time curves in the latter cases being substantially J-shaped, the temperature generated by the combustion rising rapidly soon after combustion commences. In the embodiments of the present invention described hereinafter an air gaseous fuel mixture is provided for combustion at a temperature above that at which dissociation of the fuel occurs so that rapid combustion is achieved.

Referring now to Figures 2 and 3, the illustrated apparatus comprises a chamber 10 having a circumferential wall 12 which is disposed radially outwardly of an annular inlet 14. The wall 12 slopes towards the annular inlet, and as shown comprises

a cylindrical portion 16 extending upwardly from a sloping portion 18. In the illustrated apparatus, the sloping portion 18 extends downwardly to the outer edge of the annular fluid inlet.

Within the chamber 10 there is a first annular region disposed above the annular inlet and designated 22 in Figure 2 and a second annular region 24 contiguous with the first annular region and disposed between that region and the circumferential wall 12. The second region is disposed above the sloping portion 18 of the wall in the embodiment.

The apparatus also includes means for directing fluid through the annular inlet 14 with vertical and circumferential flow components. The direction of the fluid flow through the inlet is indicated in Figure 2 by arrows 26 and 28. The flow of fluid through the inlet is such that it will move matter in the chamber 10 in a band continuously along an annular path in the regions 22, 24. This matter is moved vertically and circumferentially whilst in the first region 22 by the flow of fluid therein, is moved out of this flow of fluid in the first region into the second region by circumferential force and is directed back into the first region by the slope 18. The movement of the matter into and out of the flow of fluid is indicated by arrows 30 in Figure 2. It will be understood that whilst the matter is being circulated as indicated by arrows 30 it is also moving in the circumferential direction. Furthermore, it will be understood that when the matter moves into the outer annular region 24 it is not subjected therein to the flow of fluid and falls under gravity towards the annular inlet 14 whereupon it re-enters the fluid flow and is moved circumferentially and vertically by the fluid flow therein.

The fluid exits the chamber 10 upwardly as indicated by arrows 32 after it has passed through the annular region 22.

In the illustrated apparatus the chamber 10 includes a second circumferential wall 34 extending upwardly and disposed radially inwardly of the annular fluid inlet 14. This circumferential wall 34 has a slope towards the annular fluid inlet such that matter introduced centrally into the chamber as indicated by arrows 36 will be directed into the first annular region 22 above the annular fluid inlet 14. Whilst the whole of the second circumferential wall is provided with such a slope in the embodiment and this slope extends to the radially inner edge 38 of the annular fluid inlet 14, it is to be understood that only a portion of the circumferential wall 34 need be provided with such a slope and that slope need not extend to the edge 38.

Referring now particularly to Figures 4 to 7, the means for directing fluid through the annular inlet 14 with vertical and circumferential flow components in the illustrated apparatus comprises an

annular array of fixed inclined vanes 40 arranged in overlapping relationship, and defining therebetween respective flow passages 42 which extend vertically and circumferentially. A portion of the annular array of vanes is schematically illustrated in Figure 3, however it is to be understood that the array extends completely around the annular inlet 14.

Each vane 40 is part of a respective blade 44 which is best shown in Figure 7. Adjacent blades 44 nest together as illustrated in Figures 5 and 6 so as to dispose the vanes in overlapping relationship with the passages therebetween. Each blade 44 is also provided with respective side vanes 46 and 48 extending upwardly from radially outer and radially inner sides of its vane 40. The side vanes 46 and 48 of the blades overlap to define therebetween respective flow passages 50 and 52. The vanes 46 and 48 are inclined towards each other and the flows through the passages 50 and 52 at the radially outer and inner edges of the inlet 14, indicated by arrows 28 in Figure 2, have radially inwardly and radially outwardly flow components respectively causing the flow through the passages 42, indicated by arrow 26 in Figure 2, to be confined substantially to the annular region 22 above the vanes 40.

The blades are provided with radially outer and radially inner mounting portions 54 and 56, by which they are mounted on annular ledges 58 and 60 respectively radially outwardly and radially inwardly of the annular inlet 14. Intermediate the mounting portions the blades are provided with a ribbed portion 62 which extends vertically to the upstream ends of the vanes 40, 46 and 48. The ribs 64 of the portion 62, extend vertically and are provided on only one side of the portion 62 in the illustrated blade and define with the plain opposite side 66 of the portion 62 of an adjacent blade vertically extending flow passage means 68 communicating with the flow passages 42, 50 and 52 defined between that blade and the adjacent blade. Each blade is provided with a passage for receiving a gaseous fuel distributor, or so-called 'sparge' pipe 70. This passage comprises a bore 72 in an enlarged free end portion 74 of the mounting portion 54 and a slot 76 aligned with the bore 72 and extending therefrom through the remaining portion 78 of the mounting portion 54 into the ribbed portion 62 and terminating short of the mounting portion 56. In the ribbed portion 62 the slot is completely open at the plain side 66 thereof but bridged at spaced apart locations by the ribs 64 at the other side.

As shown in Figures 5 and 6 a pipe 70 is received in the passage therefor in alternate blades 44, each pipe being provided with radial openings arranged to supply gaseous fluid to the flow passages defined by the blade in which the pipe is

5 fitted and the blades on each side of that blade. The pipes 70 are all connected via conduit means 80 to an annular gas header tube, or manifold, 82 disposed externally of the circumferential wall 12 of the chamber.

In use heated air is caused to swirl about an annular chamber 84 beneath the annular inlet 14 and to flow through the passage means 68 defined between adjacent blades in the passages 42, 50 and 52 defined between the vanes of those blades. This air mixes with gaseous fuel from the pipes 70 to form a heated air-gaseous fuel mixture in the passage means 68 and this mixture is combusted in the annular region of 22 of the chamber 10 above the inlet 14. The air-gaseous fuel mixture is heated prior to combustion by the mixing of the gaseous fuel with the heated air to a temperature above that at which spontaneous ignition of the gaseous fuel occurs such that a rapid combustion reaction occurs as explained hereinbefore in connection with Figure 1. The rate of combustion is such that although the velocity of the air mixing with the fuel is greater than the flame propagation velocity thereof so that the resulting flow is able to move matter in a band along an annular path in the chamber 10, combustion occurs, and is substantially completed, within the extent of the band, that is before the mixture passes through the matter in the band. Additionally because the gaseous fuel is mixed with the air immediately upstream of the passages 42, most of the combustion occurs downstream of the blades 44 and accordingly they are not subjected to the full heat of the combustion reaction.

35 The above-described embodiment is particularly applicable for use in heating matter comprising a particulate material which has to be heated to a predetermined temperature which is at or below the temperature at which fast combustion reactions occur, or which is adversely affected by being continuously subjected to temperatures above that predetermined temperature during treatment.

In such an application the combustion reaction occurs substantially in the first annular region 22 in the chamber 10. The particulate matter to be heated is supplied to the chamber centrally thereof and is fed to the region 22 by the slope of the inner circumferential wall 34. This particulate material is then moved in a band continuously along an annular path in the regions 22 and 24. The particulate material is moved vertically and circumferentially by the fluid flow whilst in the first region, is moved out of the flow in the first region into the second region by circumferential force and is thereafter directed back into the first region by the slope 18 of the outer circumferential wall 12. Thus, the particulate material is moved in a band continuously around the regions 22, 24 whilst being circulated in

this band between the regions such that the material moves into and out of the heated flow during movement around the regions.

It will be appreciated that as the combustion reaction is maintained spaced from the walls 18 and 34 these are not raised to the temperature of the region 22 and therefore contact by the particulate matter of these walls does not adversely affect the matter.

Although the above-described embodiment is applicable to heating many types of particulate matter, particular examples of its application are the heating of perlite, slate and clay to expand the same.

Referring now to Figures 8 and 9, there is illustrated an apparatus for heating matter which is similar to the apparatus illustrated in Figures 2 and 3. Accordingly like reference numerals in these figures designate like or similar parts. The annular inlet 14 is spanned by an annular array of inclined vanes 86 (only a portion of the array being shown in Figure 8) which are preferably arranged in overlapping relationship for directing fluid flow into the annular zone 88 above the inlet 14 with both circumferential and vertical flow components for moving a resident bed of particulate matter in the zone 88 continuously along an annular path in a compact band 90.

Heated air is caused to swirl about annular chamber 84 beneath the inlet 14 and to flow between the vanes 86 into the zone 88. This air mixes with gaseous fuel from fuel pipes 70 immediately upstream of the vanes to form a heated air-gaseous fuel mixture which is combined in zone 88. As in the previous embodiment, the heated mixture prior to combustion is at a temperature above that at which spontaneous ignition of the gaseous fuel occurs such that a rapid combustion occurs. The rate of combustion is such that combustion is substantially completed within the extent of the band of particulate matter forming the resident bed, thus efficiently heating that matter. Further matter to be heated is either added to the resident bed or passed therethrough such that heat is transferred to the further matter from the heated particulate matter of the bed. This further matter may comprise gases, liquids or solids.

In the case where the further matter to be heated is a gas, the heated air-gaseous fuel mixture is passed through the bed along a portion of the annular extent of the zone 88 to heat the bed and the gas is passed through the bed along another portion of the annular extent of the zone 88 to be heated by the matter in the bed.

One example of solid matter which may be heated by being added to the resident bed is fine powder.

The apparatus and method described above in connection with Figures 8 and 9 may be used to heat matter, especially particulate matter directly without the use of a resident bed. In this case it will be appreciated that the matter to be heated is introduced into the zone 88 and is moved continuously along an annular path in a compact band by the passage of the heated fluid flow provided by the combustion of the heated air-gaseous fuel mixture through the matter whilst heating it.

It is to be understood that an arrangement of nested blades with fuel sparge pipes fitted to alternate blades substantially as described in connection with Figures 4 to 7 may be used in the apparatus shown in Figures 8 and 9 instead of the more simple overlapping vane arrangement schematically illustrated.

Although other gaseous fuels, such as propane, methane and vapourised oil, may be used, in the embodiments described above the gaseous fuel is natural gas and the air-natural gas mixture prior to combustion is at a temperature above 700°C. To obtain such a mixture temperature the air is preferably at a temperature of between 850 and 900°C. Other air temperatures may be used, but it has been found that at air temperatures above about 1000°C carbon deposits are likely to form in the fuel pipes 70. Thus it is advantageous to use an air temperature of less than about 1000°C.

Although the embodiments have been described utilising a heated air-gaseous fuel mixture to provide a heated flow, other combustible gaseous mixtures or gaseous mixtures which react to produce heated flow and whose reaction rate is typified by a substantially J-shaped temperature/time curve which the mixture prior to commencement of the reaction is at a temperature above that at which spontaneous ignition occurs may be used.

Claims

1. A method of heating matter comprising (i) supplying said matter to a heating zone to be heated therein and (ii) providing in said heating zone a gaseous mixture which is reactable to produce heat and igniting said gaseous mixture within the extent of said matter to thereby provide a heated fluid flow in the heating zone, characterised in that said gaseous mixture is provided in said heating zone at a temperature above that at which spontaneous ignition thereof occurs such that said gaseous mixture reacts, with no flame front being present during the reaction, within the extent of said matter.

2. A method as claimed in claim 1, wherein said gaseous mixture comprises a combustible gaseous mixture and said heat producing reaction, with no flame front present, occurring in said heating zone is a combustion reaction. 5

3. A method as claimed in claim 2, wherein said combustible gaseous mixture comprises an air-gaseous fuel mixture. 10

4. A method as claimed in claim 3, wherein the air-gaseous fuel mixture is provided at said temperature by mixing gaseous fuel with heated air. 15

5. A method as claimed in any one of the preceding claims, wherein the matter to be heated is moved in a band continuously along an annular path in an annular zone by directing fluid flow into said zone over the annular extent thereof with both circumferential and vertical flow components, said fluid flow comprising said gaseous mixture over at least a portion of the annular extent of said zone, and the reaction thereof being substantially completed within the extent of said band. 20

6. A method as claimed in claim 5, wherein said fluid flow comprises said gaseous mixture over the annular extent of said zone. 30

7. A method as claimed in claim 5 or 6, wherein said matter comprises particulate material which forms a resident bed moving in said band along said annular path. 35

8. A method as claimed in claim 6, wherein said gaseous mixture is directed into a first annular region of said annular zone, which region is contiguous with and disposed inwardly of a second annular region of said annular zone such that said reaction occurs substantially in said first annular region, and said matter is circulated between said regions whilst moving in said band. 40

9. A method as claimed in any one of claims 5 to 8 when appended to claim 3, wherein said fluid flow is directed into said annular zone through an annular inlet comprising an annular array of fixed inclined vanes, said gaseous fuel being mixed with heated air immediately upstream of respective passages defined between said vanes and wherein combustion occurs downstream of said vanes. 45

10. A method as claimed in claim 9, including confining said air-gaseous fuel mixture substantially to the region above the vanes by directing respective flows through said annular inlet at the radially inner and outer edges thereof with radially outwardly and radially inwardly flow components respectively. 50

11. A method as claimed in any one of claims 9 or 10, wherein said gaseous fuel comprises natural gas and said mixture is supplied at a temperature greater than 700 °C. 55

12. A method as claimed in claim 11, wherein said temperature of said mixture is obtained by mixing said natural gas with heated air at a temperature of less than about 1000 °C.

13. A method as claimed in claim 12, wherein said air is at a temperature of between 850 and 900 °C.

Patentansprüche

1. Verfahren zum Stoffaufheizen, das beinhaltet:
 (i) das Zuführen des Stoffs in ein Aufheizgebiet, um in diesem aufgeheizt zu werden, und
 (ii) das Vorsehen eines gasförmigen Gemisches, das reaktionsfähig ist, um Wärme zu erzeugen, im Aufheizgebiet und Entzünden des gasförmigen Gemisches in der Ausdehnung des Stoffs, um dadurch im Aufheizgebiet einen Strom von aufgeheiztem Fluid vorzusehen,
 dadurch gekennzeichnet, daß
 das gasförmige Gemisch im Aufheizgebiet bei einer Temperatur vorgesehen ist, die über der liegt, bei der seine Selbstentzündung auftritt, so daß das gasförmige Gemisch in der Ausdehnung des Stoffes reagiert, wobei während der Reaktion keine Flammenfront vorhanden ist.
2. Verfahren nach Anspruch 1, bei dem das gasförmige Gemisch ein brennbares gasförmiges Gemisch aufweist und wobei die Wärmeerzeugungsreaktion ohne Flammenfront, die im Aufheizgebiet auftritt, eine Verbrennungsreaktion ist.
3. Verfahren nach Anspruch 2, bei dem das brennbare gasförmige Gemisch ein Gemisch aus Luft und gasförmigem Kraftstoff aufweist.
4. Verfahren nach Anspruch 3, bei dem das Gemisch aus Luft und gasförmigem Kraftstoff bei der Temperatur vorgesehen wird, indem gasförmiger Kraftstoff mit aufgeheizter Luft gemischt wird.

5. Verfahren nach einem der vorhergehenden Ansprüche, bei dem der aufzuheizende Stoff in einem Band entlang eines ringförmigen Pfades in einem ringförmigen Gebiet kontinuierlich bewegt wird, indem ein Fluidstrom mit sowohl einer Umfangsströmungskomponente als auch einer vertikalen Strömungskomponente in das Gebiet über seine ringförmige Ausdehnung gelenkt wird, wobei der Fluidstrom das gasförmige Gemisch über zumindest einen Abschnitt der ringförmigen Ausdehnung des Gebietes aufweist und seine Reaktion in der Ausdehnung des Bandes im wesentlichen abgeschlossen ist.

6. Verfahren nach Anspruch 5, bei dem der Fluidstrom das gasförmige Gemisch über die ringförmige Ausdehnung des Gebietes aufweist.

7. Verfahren nach Anspruch 5 oder 6, bei dem der Stoff ein Partikelmaterial aufweist, das ein residentes Bett ausbildet, das sich im Band entlang des ringförmigen Pfades bewegt.

8. Verfahren nach Anspruch 6, bei dem das gasförmige Gemisch in einen ersten ringförmigen Bereich des ringförmigen Gebietes gelenkt wird, wobei der Bereich zu einem zweiten ringförmigen Bereich des ringförmigen Gebietes benachbart ist und sich einwärts von diesem befindet, so daß die Reaktion im wesentlichen im ersten ringförmigen Bereich auftritt, und der Stoff zwischen den Bereichen umgeführt wird, während dieser sich im Band bewegt.

9. Verfahren nach einem der Ansprüche 5 bis 8 bei Abhängigkeit von Anspruch 3, bei dem der Fluidstrom in das ringförmige Gebiet durch einen ringförmigen Einlaß gelenkt wird, der eine ringförmige Gruppe von befestigten geneigten Platten aufweist, wobei der gasförmige Kraftstoff mit der aufgeheizten Luft unmittelbar stromaufwärts von jeweiligen Kanälen gemischt wird, die zwischen den Platten definiert sind, und wobei die Verbrennung stromabwärts von den Platten stattfindet.

10. Verfahren nach Anspruch 9, das beinhaltet: das Begrenzen des Gemisches aus Luft und gasförmigem Kraftstoff im wesentlichen auf den Bereich oberhalb der Platten, indem jeweilige Ströme durch den ringförmigen Einlaß an seinen inneren und äußeren Kanten gelenkt werden, wobei radial äußere bzw. radial innere Strömungskomponenten vorhanden sind.

11. Verfahren nach Anspruch 9 oder 10, bei dem der gasförmige Kraftstoff Erdgas aufweist und

das Gemisch bei einer Temperatur zugeführt wird, die größer als 700 °C ist.

5 12. Verfahren nach Anspruch 11, bei dem die Temperatur des Gemisches erhalten wird, indem das Erdgas mit aufgeheizter Luft bei einer Temperatur von weniger als ungefähr 1000 °C gemischt wird.

10 13. Verfahren nach Anspruch 12, bei dem die Luft eine Temperatur von zwischen 850 und 900 °C hat.

Revendications

15 1. Procédé de chauffage d'une matière, comprenant les étapes consistant (i) à acheminer ladite matière jusqu'à une zone de chauffage pour qu'elle y soit chauffée, et (ii) à fournir dans ladite zone de chauffage un mélange gazeux capable de réagir pour produire de la chaleur et à enflammer ledit mélange gazeux au sein de ladite matière pour ainsi produire un courant de fluide chauffé dans la zone de chauffage, caractérisé en ce que ledit mélange gazeux est fourni dans ladite zone de chauffage à une température supérieure à celle à laquelle se produit son inflammation spontanée, de sorte que ledit mélange gazeux réagit, sans qu'aucun front de flamme ne soit présent pendant la réaction, au sein de ladite matière.

20 2. Procédé selon la revendication 1, dans lequel ledit mélange gazeux comprend un mélange gazeux combustible et ladite réaction génératrice de chaleur, sans présence d'un front de flamme, qui se produit dans ladite zone de chauffage est une réaction de combustion.

25 3. Procédé selon la revendication 2, dans lequel ledit mélange gazeux combustible comprend un mélange air-combustible gazeux.

30 4. Procédé selon la revendication 3, dans lequel le mélange air-combustible gazeux est fourni à ladite température en mélangeant un combustible gazeux à de l'air chauffé.

35 5. Procédé selon l'une quelconque des revendications précédentes, dans lequel la matière à chauffer est déplacée dans un ruban continuellement le long d'un trajet annulaire dans une zone annulaire en dirigeant un courant de fluide dans ladite zone, sur tout le volume annulaire de celle-ci, avec des composantes d'écoulement à la fois circonférentielle et verticale, ledit courant de fluide comprenant ledit mélange gazeux sur au moins une partie du

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volume annulaire de ladite zone et sa réaction étant sensiblement achevée dans le volume dudit ruban.

6. Procédé selon la revendication 5, dans lequel ledit courant de fluide comprend ledit mélange gazeux sur tout le volume annulaire de ladite zone. 5

7. Procédé selon la revendication 5 ou 6, dans lequel ladite matière comprend une matière particulière qui forme un lit résident se déplaçant dans ledit ruban le long dudit trajet annulaire. 10

8. Procédé selon la revendication 6, dans lequel ledit mélange gazeux est envoyé dans une première région annulaire de ladite zone annulaire, laquelle région est contiguë à une deuxième région annulaire de ladite zone annulaire, et disposée à l'intérieur de cette deuxième région, de sorte que ladite réaction se produit sensiblement dans ladite première région annulaire et que ladite matière est mise en circulation entre lesdites régions pendant qu'elle se déplace dans ledit ruban. 15
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9. Procédé selon l'une quelconque des revendications 5 à 8 quand elles dépendent de la revendication 3, dans lequel ledit courant de fluide est envoyé dans ladite zone annulaire à travers une entrée annulaire comprenant une série annulaire d'aubes fixes inclinées, ledit combustible gazeux étant mélangé avec de l'air chauffé immédiatement en amont de passages respectifs définis entre lesdites aubes, et dans lequel la combustion se produit en aval desdites aubes. 30
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10. Procédé selon la revendication 9, comprenant l'étape consistant à confiner ledit mélange air-combustible gazeux sensiblement à la région qui surmonte les aubes en dirigeant des courants respectifs à travers ladite entrée annulaire, au droit de ses bords radialement intérieur et extérieur, avec des composantes d'écoulement respectivement orientées radialement vers l'extérieur et radialement vers l'intérieur. 40
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11. Procédé selon l'une quelconque des revendications 9 et 10, dans lequel ledit combustible gazeux comprend du gaz naturel et ledit mélange est délivré à une température supérieure à 700 °C. 50

12. Procédé selon la revendication 11, dans lequel ladite température dudit mélange est obtenue en mélangeant ledit gaz naturel avec de l'air chauffé à une température de moins d'environ 1000 °C. 55

13. Procédé selon la revendication 12, dans lequel ledit air est à une température entre 850 et 900 °C.

FIG. 1

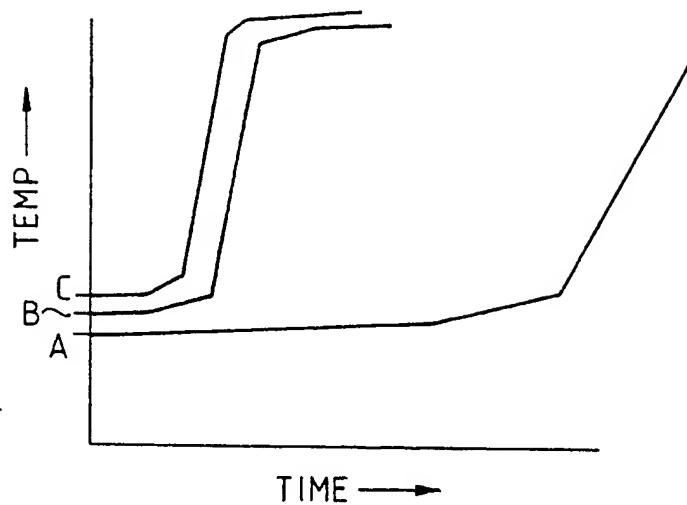


FIG. 7

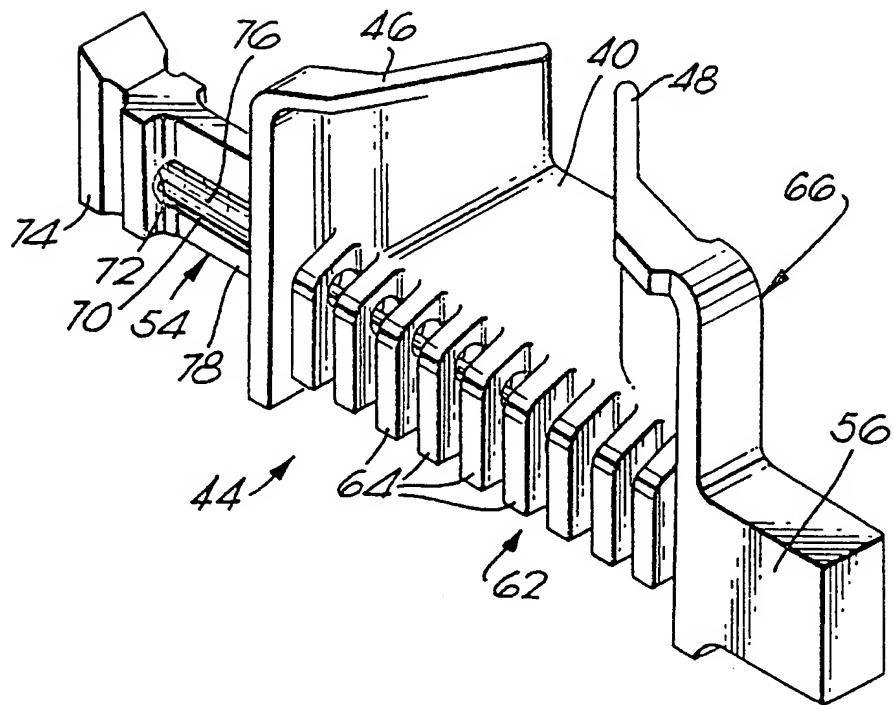


FIG. 2

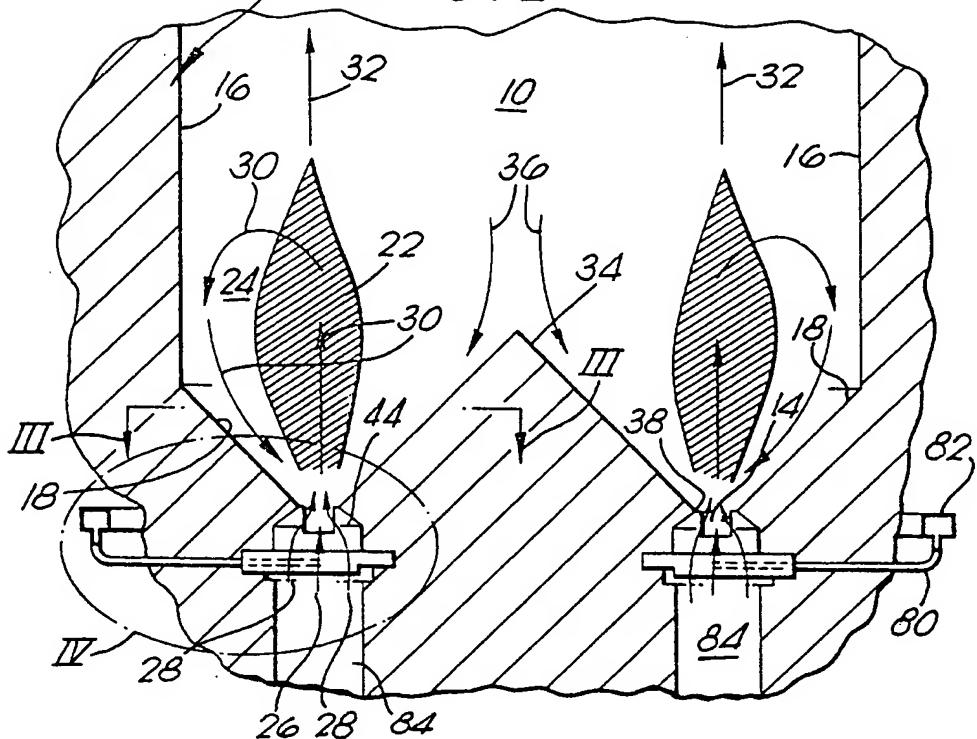
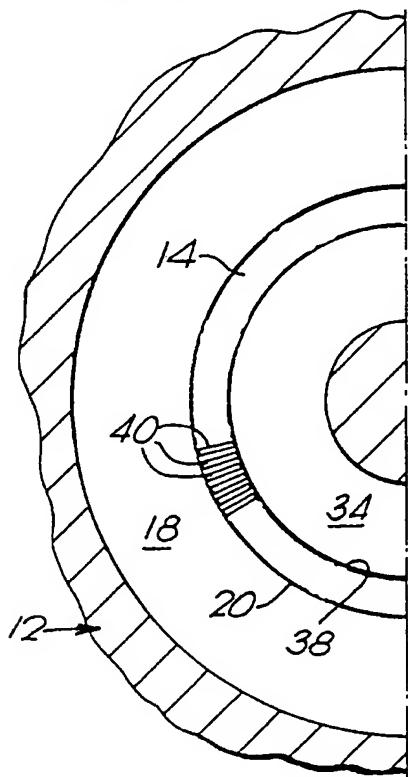
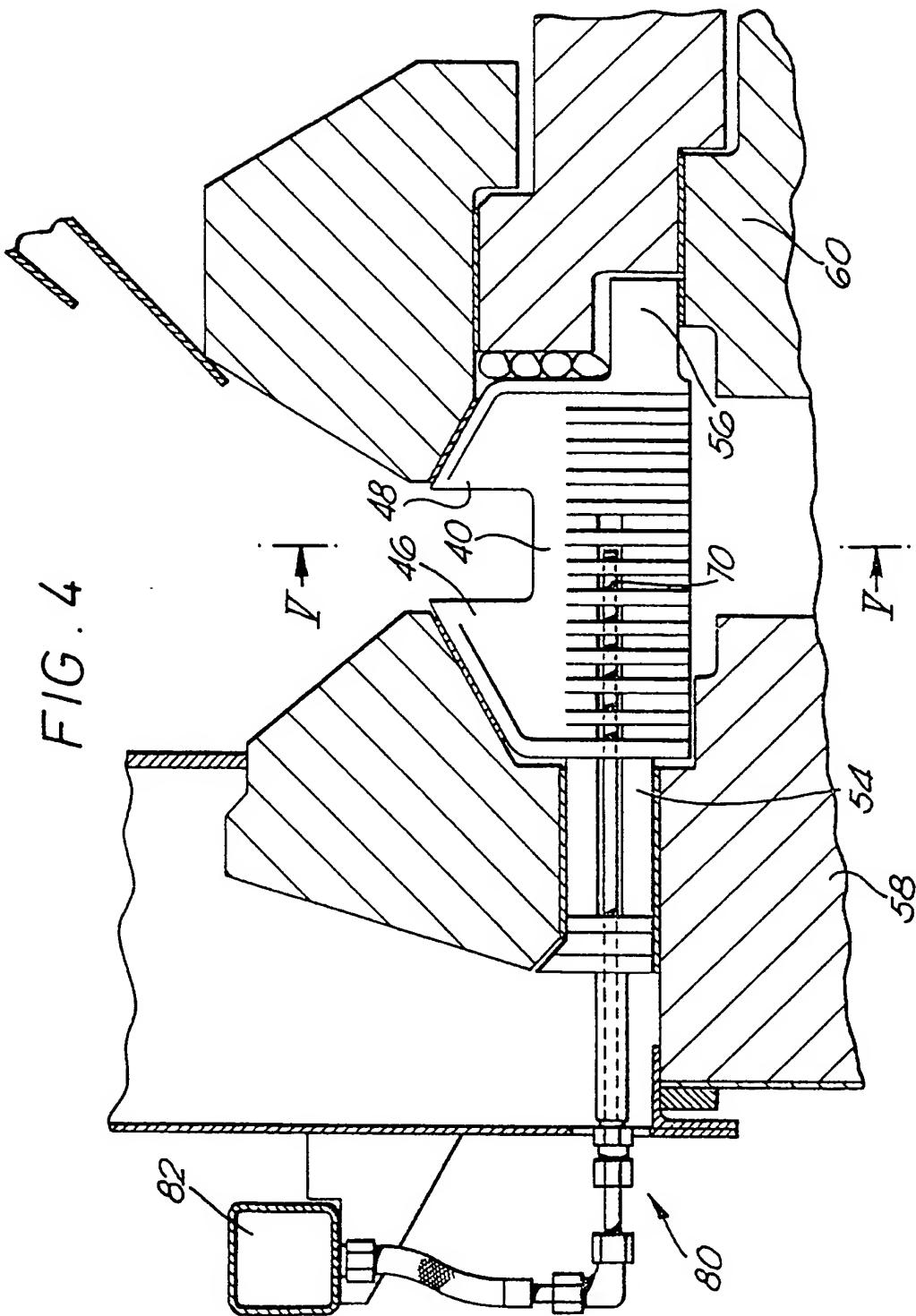


FIG. 3





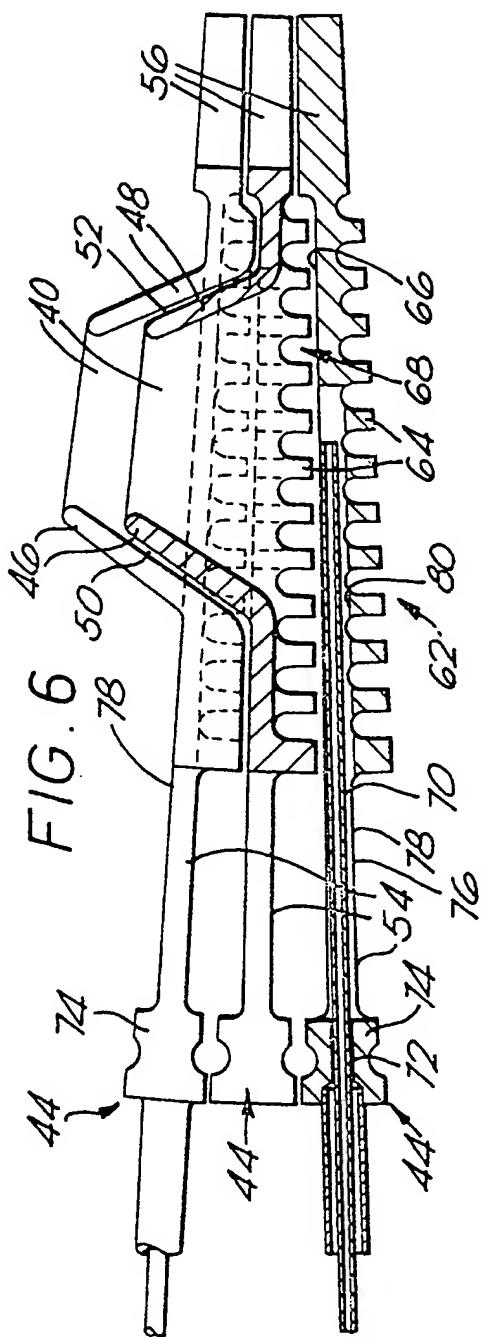


FIG. 5

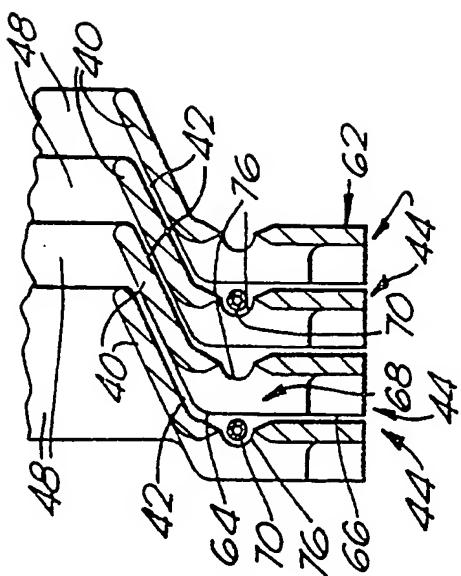


FIG. 9

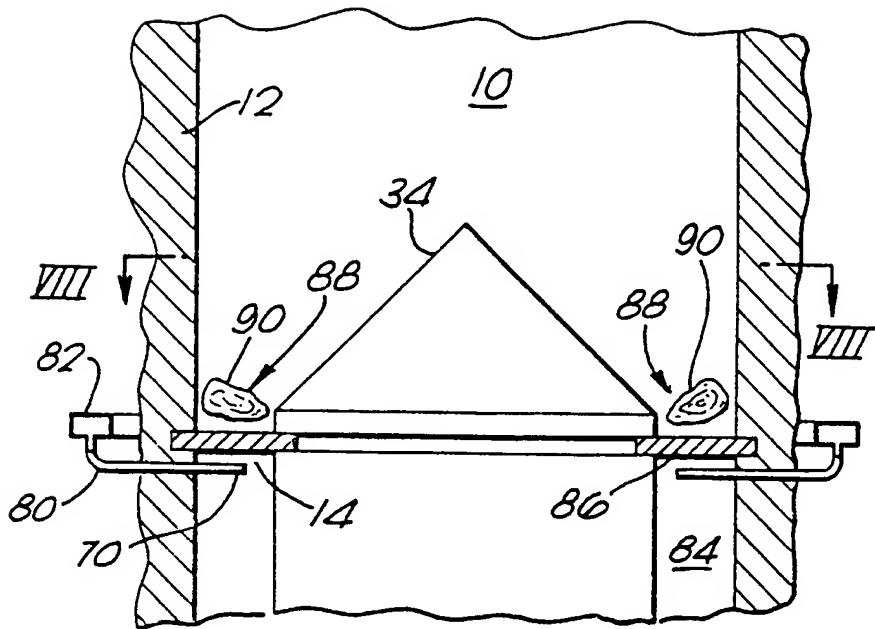


FIG. 8

